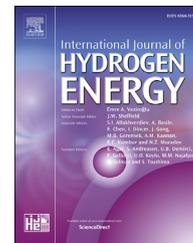




ELSEVIER

Available online at [www.sciencedirect.com](http://www.sciencedirect.com)

ScienceDirect

journal homepage: [www.elsevier.com/locate/he](http://www.elsevier.com/locate/he)

# Evidence for hydrogenase-4 catalyzed biohydrogen production in *Escherichia coli*

Satenik Mirzoyan<sup>a</sup>, Pablo Maria Romero-Pareja<sup>a,b</sup>, Maria Dolores Coello<sup>b</sup>, Armen Trchounian<sup>a</sup>, Karen Trchounian<sup>a,\*</sup>

<sup>a</sup> Department of Biochemistry, Microbiology and Biotechnology, Faculty of Biology, Yerevan State University, 0025, Yerevan, Armenia

<sup>b</sup> Department of Environmental Technology, Universidad de Cádiz, Poligono Rio San Pedro S/n, 11510, Puerto Real, Cadiz, Spain

## ARTICLE INFO

### Article history:

Received 18 June 2017

Received in revised form

15 July 2017

Accepted 17 July 2017

Available online 1 August 2017

### Keywords:

*Escherichia coli*

Hydrogenases

Glycerol, glucose and formate utilization

Bioenergy and biohydrogen

pH

## ABSTRACT

Biohydrogen production by *Escherichia coli* during fermentation of the mixture of glycerol, glucose and formate at different pH values was studied. Employing mutants lacking large subunits of different hydrogenases (Hyd), it was reported that, at pH 7.5, H<sub>2</sub> production was produced except in a *hyaB hybC hycE* triple mutant, thus suggesting compensatory H<sub>2</sub>-producing functions of the Hyd enzymes. Activity of Hyd-4 was revealed in glucose assays at pH 7.5 in the triple mutant whereby 62% of the wild type level of H<sub>2</sub> production was derived from Hyd-4. In formate assays, it was shown, that, first, the *hyaB hybC* double mutant had a H<sub>2</sub> production ~3 fold higher than wild type, indicating that Hyd-1 and Hyd-2 oxidize H<sub>2</sub>, and second, that at pH 5.5, Hyd-4 and Hyd-3 were responsible for H<sub>2</sub> production. These findings are significant when applying various carbon sources such as sugars, alcohol and organic acids for biohydrogen production.

© 2017 Hydrogen Energy Publications LLC. Published by Elsevier Ltd. All rights reserved.

## Introduction

The current climate of shrinking fossil fuel resources and continually increasing energy demand requires the identification of efficient, renewable and ecologically friendly new sources of energy. Molecular hydrogen, or dihydrogen (H<sub>2</sub>), fits these criteria, with its high energy density – 142 kJ/g, and having water as only product of combustion [1,2]. H<sub>2</sub> is produced during dark fermentation by bacteria through biological conversion of organic substrates such as alcohols (glycerol),

organic carboxylic acids (e.g. acetic, formic, succinic acids), different sugars (e.g. glucose, lactose, xylose), which are present in organic wastes originating from agricultural and industrial processes [3,4]. Glycerol is massively produced as a by-product during biodiesel generation (1 kg of glycerol is produced for every 10 kg of biodiesel synthesized) [5]. Different sugars and organic acids (e.g. acetic, formic, succinic) are present in agricultural and industrial wastes, making these potentially valuable energy sources [6–9].

Gonzalez et al. [10] reported a decade ago that polyols, such as glycerol, can be metabolized under anaerobic fermentative

\* Corresponding author. Department of Biochemistry, Microbiology and Biotechnology, Yerevan State University, 1 A. Manoogian Str., 0025, Yerevan, Armenia.

E-mail address: [k.trchounian@ysu.am](mailto:k.trchounian@ysu.am) (K. Trchounian).

<http://dx.doi.org/10.1016/j.ijhydene.2017.07.126>

0360-3199/© 2017 Hydrogen Energy Publications LLC. Published by Elsevier Ltd. All rights reserved.

conditions by *Escherichia coli* at pH 6.3 and further, at pH 7.5 [11]. Products of the process depend on external pH but biohydrogen was always detected. As a consequence of such a significant finding, different mixtures of inexpensive and readily available carbon sources such as sugars (lactose, xylose etc.) and glycerol have been tested to improve H<sub>2</sub> production by *Escherichia coli* [12–15]. Moreover, different mixtures of carbonaceous substrates have been tested by various research groups in co-cultivation experiments with the aim of transformation these organic substrates into valuable chemicals [16–18].

During mixed acid fermentation *E. coli* produces H<sub>2</sub> at different pHs. H<sub>2</sub> is produced via membrane-bound [Ni–Fe] hydrogenase (Hyd) enzymes. Their activation depends on various external factors such as the type of fermentation substrate, external pH etc. [19–22]. The mechanisms underlying the expression of genes encoding the Hyd enzymes and, furthermore, their posttranslational maturation, assembly and activity, as well as reciprocal interaction with other membrane proteins are an intense focus of study. An important feature of Hyd enzymes in *E. coli* is their reversibility with regard to H<sub>2</sub> production and oxidation [9,19]. The main H<sub>2</sub> evolving formate hydrogen lyase (FHL-1) complex consists of Hyd-3 and formate dehydrogenase (FDH-H), is active at low pH [19]. The other formate hydrogen lyase complex – FHL-2 formed by Hyd-4 and FDH-H is proposed to be active at high pH [23]. Although, it is well documented [24–26] that synthesis of both FHL complexes is under transcriptional control, their differential synthesis is not clearly defined.

External pH is important for the activity of Hyd enzymes [27,28], which makes a key contribution to the enhancement of H<sub>2</sub> production. Moreover, in the case of Hyd-4 activity, the fermentation substrate is important, as well as its concentration. Thus, Hyd-4 is active within a glucose concentration range from low to moderately high (0.2%) [22]. Several other considerations are highly relevant for enhancing biohydrogen generation, including understanding the physiology of the Hyd enzymes, the involvement of heavy metals and stimulating and inhibiting metabolites [15,29–31]. Moreover, the choice of strains, and whether the genes encoding some of the Hyd enzymes and their regulatory proteins are absent, has a major influence on H<sub>2</sub> production [32,33].

Currently, a key issue in the field of biohydrogen production is the fermentation or utilization of various mixed carbon sources released from wastes of industry or agriculture. Other major goals are the assessment and the improvement of the process of H<sub>2</sub> production and a major aim is to understand what controls the activity of Hyd enzymes.

Fermentation of a combination of three carbon sources (glucose, glycerol and formic acid) by *E. coli*, which constitutes itself a novel approach, with different external pHs, is conducted in the current work, targeting conditions for enhancement of H<sub>2</sub> production and on providing further insights into the Hyd enzymes involved in H<sub>2</sub> generation.

## Materials and Methods

### Bacterial strains and cultivation

The characteristics of *E. coli* strains used in the study, BW25113 or MC4100 (wild type parents) and mutant strains with defects in the genes coding Hyd enzymes are described in Table 1.

Bacterial cells culture was grown overnight (O/N) under anaerobic fermentative conditions and transferred into buffered growth medium containing peptone (20 g L<sup>-1</sup>) at pH of 7.5, 6.5 and 5.5, with salt compositions as follow: 15 g L<sup>-1</sup> K<sub>2</sub>HPO<sub>4</sub>, 1.08 g L<sup>-1</sup> KH<sub>2</sub>PO<sub>4</sub> and 5 g L<sup>-1</sup> NaCl (pH 7.5); 7.4 g L<sup>-1</sup> K<sub>2</sub>HPO<sub>4</sub>, 8.6 g L<sup>-1</sup> KH<sub>2</sub>PO<sub>4</sub> and 5 g L<sup>-1</sup> NaCl (pH 6.5), and 1.08 g L<sup>-1</sup> K<sub>2</sub>HPO<sub>4</sub>, 15 g L<sup>-1</sup> KH<sub>2</sub>PO<sub>4</sub> and 5 g L<sup>-1</sup> NaCl (pH 5.5). The medium was simultaneously supplemented with the following carbon sources: glucose (2 g L<sup>-1</sup>), glycerol (10 g L<sup>-1</sup>) and sodium formate (0.68 g L<sup>-1</sup>). Kanamycin (25 μl mL<sup>-1</sup>) was also added when appropriate (see Table 1).

Bacterial cultures were grown in sealed flasks with closed lids under fermentative conditions for 18–24 h at 37 °C; anaerobic conditions in the medium were achieved by displacing O<sub>2</sub> during autoclaving [11,21,22]. The medium pH was determined using a pH-meter with selective pH-electrode (HJ1131B, Hanna Instruments, Portugal) and adjusted to required values (see above) with 0.1 M NaOH or 0.1 N HCl. Bacterial growth was monitored by means of measuring bacterial culture absorbance by spectrophotometric method (600 nm) (Spectro UV–Vis Auto, Labomed, USA).

**Table 1 – Characteristics of *E. coli* wild type parents and mutant strains used.**

Strains	Genotype	Absent hydrogenase subunit or related protein	References
BW25113	<i>lacI<sup>q</sup> rrmB<sub>T14</sub> ΔlacZ<sub>W116</sub> hsdR514 ΔaraBAD<sub>AH33</sub> Δrha BAD<sub>LD78</sub></i>	Wild type parent	[11]
MC4100	<i>F-araD139 Δ (argF-lac)U169 λ-rpsL150 relA1 deoC1 flhD5301 Δ (fruK-yeiR)725 (fruA25) rbsR22 Δ (fimB-fimE) 632 (::IS1)</i>	Wild type parent	[21,34]
JW0955 Km <sup>Ra</sup>	BW 25113 Δ <i>hyaB</i>	Large subunit of Hyd-1	[11,28]
JW2962 Km <sup>Ra</sup>	BW 25113 Δ <i>hybC</i>	Large subunit of Hyd-2	[11,28]
JW 2691 Km <sup>Ra</sup>	BW 25113 Δ <i>hycE</i>	Large subunit of Hyd-3	[35]
JW2472 Km <sup>Ra</sup>	BW25113 Δ <i>hyfG</i>	Large subunit of Hyd-4	[9,37]
MW 1000	BW25113 Δ <i>hyaB</i> Δ <i>hybC</i> ;	Large subunits of Hyd-1 and Hyd-2	[9,37]
FTD147	MC4100 Δ <i>hyaB</i> Δ <i>hybC</i> Δ <i>hycE</i>	Large subunits of Hyd-1, Hyd-2 and Hyd-3	[26]
FTD150	MC4100 Δ <i>hyaB</i> Δ <i>hybC</i> Δ <i>hycE</i> Δ <i>hyfG</i>	Large subunits of Hyd-1, Hyd-2, Hyd-3 and Hyd-4	[26]

<sup>a</sup> Resistant to kanamycin.

### Redox potential determination and hydrogen production assays

Redox potential ( $E_h$ ) in bacterial biomass was determined using two different redox, titanium-silicate (Ti–Si) (EO-02, Gomel State Enterprise of Electrometric Equipment (GSEEE), Gomel, Belarus) and platinum (Pt) (EPB-1, GSEEE, or PT42BNC, Hanna Instruments, Portugal) glass electrodes [11,21,36,37]. The Ti–Si-electrode measures the overall  $E_h$ , whereas the Pt-electrode is responsive to  $H_2$  under anaerobic conditions [38]. This characteristic of the dual electrode system (Ti–Si/Pt) has been used [19,21,36,37] to detect  $H_2$  gas production in bacterial biomass, by measuring the  $H_2$  production rate ( $V_{H_2}$ ) of bacteria calculated as the difference between the initial rates of decrease in Pt- and Ti–Si-electrodes readings and expressed in mV of  $E_h$  per min per mg dry weight of bacteria. This electrochemical approach applied for hydrogen determination is similar to the Clark-type electrode used by Fernandez [39] and other researchers [40,41]. As a control experiment were used cells without any addition of carbon source. In this case no any  $H_2$  production has been detected. Importantly, salt content of the solution does not affect the evolution of  $E_h$  by  $H_2$  saturation [42], and, moreover, supplementation of  $H_2$  into the solution does not have any impact on external or medium pH [42]. In conclusion, the method with two redox electrodes for determining  $H_2$  production by bacteria is well established and validated [19,21,36,37].  $V_{H_2}$  is recalculated and expressed as  $\text{mmol } H_2 \text{ min}^{-1} (\text{g dry weight})^{-1}$ .

The  $E_h$  measurements were performed in the assay buffer solution (150 mM Tris-phosphate, at the indicated pH, including 0.4 mM  $MgSO_4$ , 1 mM NaCl and 1 mM KCl) to determine  $H_2$  production upon glucose (glucose assay), glycerol (glycerol assay) or formate (formate assay) addition. Glucose, glycerol or formate were added for assays at similar concentrations as used for cell cultivation.

$H_2$  generation by cells was independently checked by chemical [21,22,36,37,43] and microbiological methods using Durham test tubes [21].

### Chemicals, data analysis and cell preparation

Bacterial whole cells and dry weight of cell mass were determined as described previously [8,10,17,19,21,46–48]. All reagents and chemicals used for experiments were of analytical grade (Sigma Aldrich, Carl Roth GmbH, Germany).

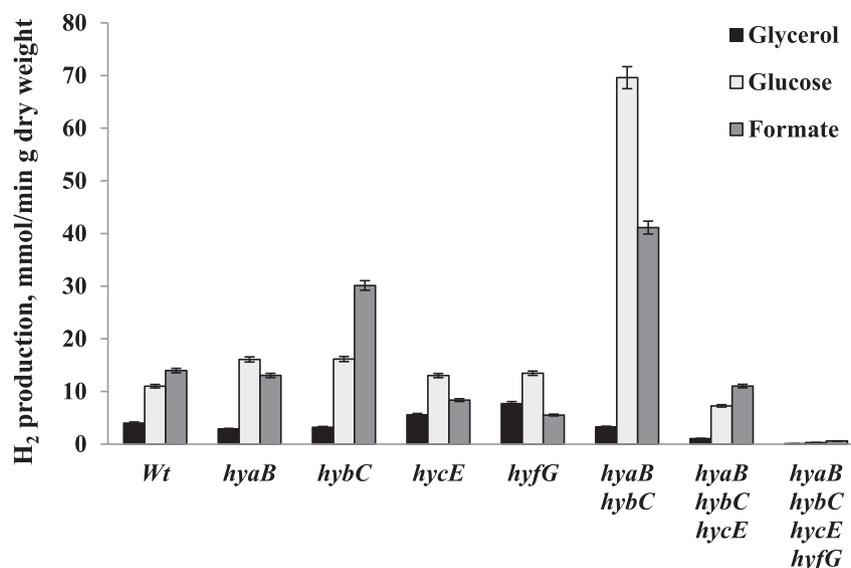
All measurements were performed in triplicate. Figures show average values. The standard errors were calculated [19,21,37] and mention was only made for values over 3%. Statistical significance of experimental assays were confirmed if  $p < 0.01$ ; otherwise, the results were considered not valid if  $p > 0.5$  [19,21,37].

## Results and discussion

### $H_2$ production during utilization of glucose, glycerol and formate mixture at slightly alkaline pH

It has been well reported [11,19–21] that *E. coli* is able to use glucose and formic acid under anaerobic fermentative conditions producing  $H_2$  at different external pHs. More recently [10,18–20], it was also confirmed that *E. coli* is able to ferment glycerol at different pHs generating  $H_2$ .

To determine the role of different Hyd enzymes in  $H_2$  producing metabolic pathways during utilization of various carbon sources (glucose, glycerol and formate), the  $H_2$  production by different *E. coli* Hyd mutants was conducted and compared with the wild type strain. Note, that all three carbon sources were added simultaneously in the growth medium for obtaining cell biomass. After harvesting the cells,  $H_2$  production assays were performed (see Materials and methods). In



**Fig. 1** –  $H_2$  production rate ( $V_{H_2}$ ) by the *E. coli* BW25113 wild type parent and mutant strains with various defects in Hyd-1 to 4 during mixed carbon sources fermentation in the assays supplemented with glycerol, glucose or formate at pH 7.5. For strains used see Table 1; for others, see Materials and Methods.

BW25113 wild type (Fig. 1) or MC4100 (not shown) in glycerol assays at pH 7.5,  $V_{H_2}$  was  $\sim 4$  mmol  $\text{min}^{-1}$  (g dry weight) $^{-1}$ . Similar  $V_{H_2}$  (see Fig. 1) was determined for single and double mutant strains devoid of large subunits of Hyd-1 and/or Hyd-2 (*hyaB*, *hybC* and *hyaB hybC*, see Table 1). As observed in Fig. 1, the assay of the *hyfG* mutant revealed a  $\sim 2$  fold increase in  $V_{H_2}$  suggesting that under these conditions (glycerol assay, pH 7.5) Hyd 4 functions in the  $H_2$  uptake direction. As several enzymes are present, a single Hyd enzyme could not be considered to be solely responsible for the  $H_2$  production. For example, Hyd-2 and Hyd-1 have been determined to be responsible for  $H_2$  production and Hyd-3 and Hyd-4 for  $H_2$  oxidation [11,19] during glycerol only fermentation.

To further understand the role of the Hyd-4 enzyme in  $H_2$  metabolism under these conditions, the FTD147 triple and FTD150 quadruple mutants with defects in large subunits of Hyd-1 to Hyd-3, and Hyd-1 to Hyd-4, respectively (see Table 1) were assayed for  $H_2$  production at pH 7.5. In FTD147 the assay with glycerol revealed that  $V_{H_2}$  was decreased  $\sim 4$  fold compared with wild type and negligible in FTD150 (see Fig. 1), indicating that  $H_2$  production was hardly affected unless deletions of genes for three or four Hyd enzymes were introduced. Moreover, the results for FTD147 indicate that Hyd-4 must be responsible for the residual  $H_2$  production. The results obtained also suggest that, in the wild type, after mixed carbon-source fermentation and using glycerol in assays, each Hyd enzyme can potentially compensate for the absence or lack of activity of others in the  $H_2$  production direction, and that the different enzymes are reversible during the fermentation under these conditions. Moreover, this shows that only when activity of minimally three of the Hyd enzymes is disturbed can  $H_2$  production be abolished. This compensatory mechanism and inter-dependence between Hyd enzyme activities has been proposed previously for other conditions [3,44], suggesting that  $H_2$  cycling might be a common phenomenon for anaerobic fermentation in many cases. Probably  $H_2$  cycling pathways act towards maintaining cytoplasmic pH and, thus, proton motive force [44].

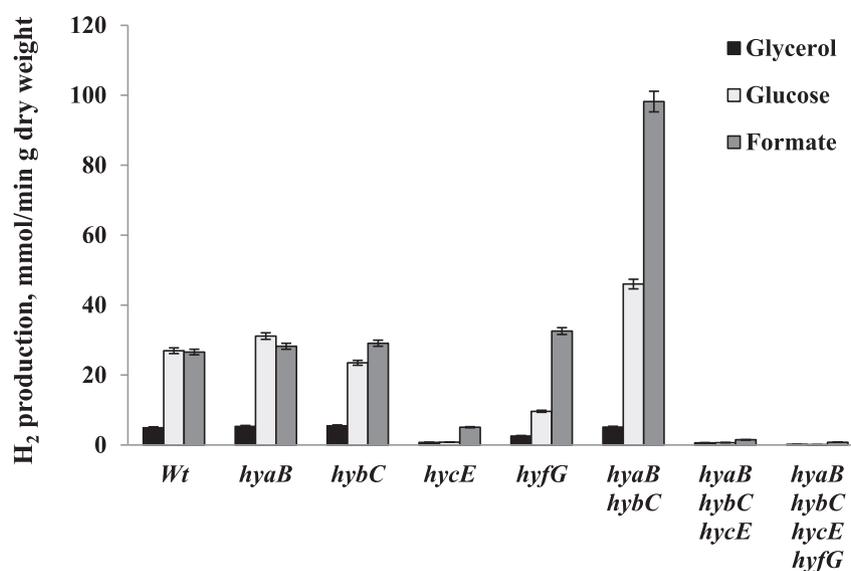
Biohydrogen production rate by wild type cells was doubled at pH 7.5 in the glucose assay in comparison to supplementation of glycerol (see Fig. 1). The observed increase of  $V_{H_2}$  in glucose assays with either single or double mutant versus production of wild type revealed which Hyd enzymes were working in  $H_2$  oxidation direction. The increase in  $V_{H_2}$  was especially significant for the *hyaB hybC* double mutant, being of  $\sim 6.3$  fold higher (see Fig. 1).  $V_{H_2}$  in the *hyaB hybC hycE* triple mutant decreased only slightly ( $\sim 1.5$  fold), indicating that Hyd-4 was responsible 62% of the  $H_2$  production under these conditions. This was confirmed by analysis of the FTD150 mutant (with absence of large subunits of Hyd-1 to 4, see Table 1) where  $H_2$  production was essentially null. Based on the observation of the large decrease ( $\sim 10$  fold) in  $V_{H_2}$  when comparing the *hyaB hybC hycE* triple mutant and the *hyaB hybC* double mutant, it can be confirmed also that Hyd-3 also makes a major contribution towards  $H_2$  production. This enzyme was previously assigned to be the main contributor for  $H_2$  production during dark fermentation with only glucose as carbon source, regardless of pH [45]. However, activity in the reverse direction, i.e.  $H_2$  uptake, was also observed during glucose fermentation for Hyd-3 [46]. Moreover, at pH 7.5  $H_2$  uptake

activity was observed for Hyd-1 and Hyd-2 in glucose assays, the latter having been previously reported to act in this direction at pH 5.5 [27,28]. The increased  $H_2$  production in the *hyaB hybC* double mutant might be also due to the fact that there is more capacity for the cofactor biosynthetic machinery to mature more  $H_2$  producing Hyd-3 and Hyd-4 enzymes [47,48].

Interestingly, whereas lack of Hyd-1 had a negligible effect in the formate assay on  $H_2$  metabolism and evolution, in the *hybC* mutant (Hyd-2 deficient)  $V_{H_2}$  was increased  $\sim 2.2$  fold (Fig. 1). The increase in the  $V_{H_2}$  for the *hyaB hybC* double mutant with formate and glucose assays were similar ( $\sim 3$  fold), when compared to wild type (see Fig. 1). When the formate assays were performed in *hycE* or *hyfG* single mutants,  $H_2$  production at pH 7.5 was reduced  $\sim 1.7$  and  $\sim 2.5$  fold, respectively (see Fig. 1). These results might point to a net  $H_2$  production activity of Hyd-3 and Hyd-4 upon formate supplementation, which may be justified by the fact that formate is a weak acid and functions as an uncoupler. In such an instance, the cells need to export it into external medium for maintaining stable cytoplasmic pH via Hyd enzymes resulting in  $H_2$  production. Again, it was observed that Hyd-4 was also responsible for  $H_2$  production in the formate assay, as  $V_{H_2}$  only decreased  $\sim 1.3$  fold in the triple mutant. This observation, similar to that registered in glucose assay, implies a new role for Hyd-4 activity in the absence of the other three Hyd enzymes, which was not detected when cells were grown during glucose only fermentation [26]. Addition of glucose, glycerol or formate in the assays at pH 7.5 revealed the ability for a dual role of the same Hyd enzyme, confirming the reversibility and the activation of all enzymes.

#### *H<sub>2</sub> production during utilization of glucose, glycerol and formate mixture at slightly acidic pH*

*E. coli* wild type showed a similar  $V_{H_2}$  for the glycerol assay at pH 7.5 and 6.5 (Figs. 1 and 2).  $H_2$  production decreased only in the *hycE* or *hyfG* single mutants ( $\sim 6.8$  and  $\sim 2$  fold, respectively), compared to wild type (see Fig. 2), suggesting that Hyd-3 and/or Hyd-4 are responsible for  $H_2$  production at pH 6.5. Surprisingly, Hyd-3 was the only enzyme responsible for  $H_2$  production during glycerol only fermentation [49]. Interplay between different enzymes might be different at pH 6.5 and at pH 7.5, given that at pH 6.5 no compensatory uptake or producing functions are present. The finding that a similar  $H_2$  production rate in FTD147 and *hycE* mutants (see Fig. 2) supports the mentioned role of Hyd-3 and Hyd-4 in  $H_2$  production direction. Similar trends to glycerol were observed for the glucose assay, with perhaps a more marked  $H_2$  production role for the Hyd-3 enzyme (see Fig. 2), as shown in the *hycE* mutant where  $V_{H_2}$  decreased to a greater extent compared to wild type than in *hyfG* mutant, where it decreased by  $\sim 2.8$  fold (see Fig. 2). In contrast to the glycerol assay,  $H_2$  production increased in *hyaB hybC* double mutant ( $\sim 1.7$  fold, Fig. 2) suggesting that these enzymes are working in the  $H_2$  uptake mode. Although comparable results were obtained for formate and glucose assay in *hyaB* and *hybC* single mutants, an important difference between these assays was the increase in  $V_{H_2}$  in the *hyfG* mutant compared to wild type ( $\sim 1.3$  fold, Fig. 1) suggesting a new formate dependent  $H_2$  oxidizing



**Fig. 2** – H<sub>2</sub> production rate ( $V_{H_2}$ ) by the *E. coli* BW25113 wild type parent and mutant strains with various defects in Hyd-1 to 4 during mixed carbon sources fermentation in the assays supplemented with glycerol, glucose or formate at pH 6.5. For other information see legend to Fig. 1.

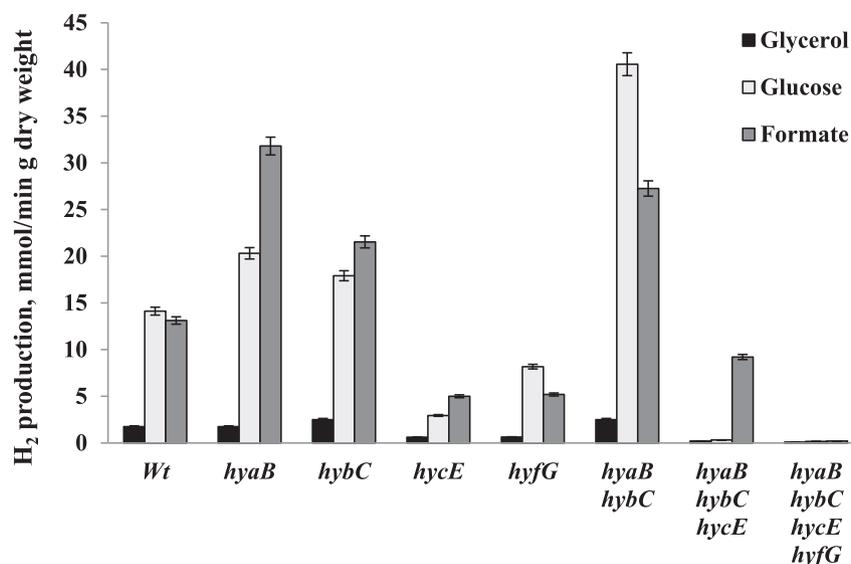
Hyd-4 activity. This observation for Hyd-4 is new and potentially adds new insights into understanding the regulation of Hyd enzyme activity and H<sub>2</sub> cycling.

It is concluded that for continuous H<sub>2</sub> production, the activity of two Hyd enzymes might be important, and Hyd-3 and Hyd-4 seem to such a pair of such enzymes establishing a H<sub>2</sub> cycle in both directions: producing and oxidizing H<sub>2</sub>, respectively. When the *hyfG* mutant was grown on glycerol and formate mixture, or on glucose only, and employed consequently for formate assays, no activity or contribution of Hyd-4 in H<sub>2</sub> metabolism and evolution was found [1,3]. Clearly, therefore, the carbon source added to the assays has clear

effect on total Hyd enzyme activity whose suggested function is to maintain the H<sub>2</sub> cycle and cytoplasmic pH.

#### H<sub>2</sub> production during utilization of glucose, glycerol and formate mixture at acidic pH

H<sub>2</sub> production by *E. coli* during mixed carbon source fermentation in wild type cells at pH 5.5 upon glycerol supplementation was the same as at pH 6.5 and pH 7.5 (comp. Fig. 3 with Figs. 1 and 2). However, in glucose-supplemented assays it was comparable only to pH 7.5 (see Figs. 1–3). Glycerol assay of *hycE* or *hyfG* single mutants resulted in a similar  $V_{H_2}$



**Fig. 3** – H<sub>2</sub> production rate ( $V_{H_2}$ ) by the *E. coli* BW25113 wild type parent and mutant strains with various defects in Hyd-1 to 4 during mixed carbon sources fermentation in the assays supplemented with glycerol, glucose or formate at pH 5.5. For other information see legend to Fig. 1.

decrease of ~3 fold compared to wild type (see Fig. 3). No role for Hyd-1 or Hyd-2 was detected, which is in contrast with the fact that the same Hyd enzymes were reported as responsible for H<sub>2</sub> oxidation when grown on glycerol only [49].

Hydrogen production in glucose assays was strongly Hyd-3 but not Hyd-4 dependent. That is inferred from the following observations: decrease of V<sub>H2</sub> in *hycE* compared to wild type (~4.8 fold) and negligible H<sub>2</sub> production in *hyaB hybC hycE* mutant (see Fig. 3). The main H<sub>2</sub> uptake activity is contributed by Hyd-1 in glucose assay.

H<sub>2</sub> production in formate assays was similar in wild type cells at pH 5.5 and pH 7.5, but not at pH 6.5 (see Fig. 1). Moreover, in *hycE* or *hyfG* single mutants H<sub>2</sub> production was decreased ~2.6 fold, and in *hyaB hybC* double mutant V<sub>H2</sub> was increased ~2.1 fold, compared to wild type. Taken together it can be concluded that Hyd-3 and Hyd-4 were responsible for H<sub>2</sub> production upon formate supplementation, probably for neutralization of formate via FHL complex.

As reported for other pHs, during mixed carbon sources fermentation at pH 5.5 the activities of Hyd enzymes differ depending on the substrate added. The clear difference might be explained via physiological conditions and requirements of the cell to act in one or another direction. So, for example when a weak acid such as formate is externally added, the cells act to neutralize it and switch two using Hyd enzymes (Hyd-3 and 4) for neutralization via H<sub>2</sub> production. A relevant consequence is that Hyd-4 is also formate-dependent at pH 5.5.

## Conclusions and significance

The physiological direction of Hyd enzymes is affected by the 4fermentation carbon sources. In particular, formate-dependent Hyd-4 activity was demonstrated. At low pH in formate assays mainly Hyd-4 was responsible for H<sub>2</sub> production. Enhanced H<sub>2</sub> production was detected in formate-supplemented assays when Hyd-1 and Hyd-2 activity were absent.

Thus, all Hyd enzymes can either work in H<sub>2</sub> uptake or production directions at a wide range of external pH depending on the carbon source added. They are likely to regulate the pH gradient across the membrane via producing or taking up H<sub>2</sub>. It is suggested that Hyd enzymes are proton sensors and act in H<sub>2</sub> production or uptake direction when the pH or proton concentration inside or outside the cell are changed.

The results pointed out compensatory producing functions of Hyd enzymes in the presence of glycerol and thus only disturbance of H<sub>2</sub> cycling decreased H<sub>2</sub> production. These findings provide an essential understanding when applying various bacteria or biomass to generate energy sources during dark fermentation via utilization of different organic waste materials.

## Acknowledgements

The study was supported by Armenian National Science and Education Fund (ANSEF, USA) Research grant to KT (Biotech-4184) and Research grant from State Committee on Science,

Ministry of Education and Science of Armenia, to AT (15T-1F123).

## REFERENCES

- [1] Trchounian K, Trchounian A. Hydrogen production from glycerol by *Escherichia coli* and other bacteria: an overview and perspectives. *Appl Energy* 2015;156:174–84.
- [2] Hosseini SE, Wahid MA. Hydrogen production from renewable and sustainable energy resources: promising green energy carrier for clean development. *Renew Sustain Energy Rev* 2016;57:850–66.
- [3] Trchounian K, Trchounian A. *Escherichia coli* hydrogen gas production from glycerol: effects of external formate. *Renew Energy* 2015;83:345–51.
- [4] Chatellard L, Marone A, Carrère H, Trably E. Trends and challenges in biohydrogen production from agricultural waste. In: *Biohydrogen production: sustainability of current technology and future perspective*. Springer India; 2017. p. 69–95.
- [5] Scott SA, Davey MP, Dennis JS, Horst I, Howe CJ, Lea-Smith DJ, et al. Biodiesel from algae: challenges and prospects. *Curr Opin Biotechnol* 2010;21:277–86.
- [6] Ghimire A, Frunzo L, Pirozzi F, Trably E, Escudie R, Lens PN, et al. A review on dark fermentative biohydrogen production from organic biomass: process parameters and use of by-products. *Appl Energy* 2015;144:73–95.
- [7] Sargsyan H, Trchounian K, Gabrielyan L, Trchounian A. Novel approach of ethanol waste utilization: biohydrogen production by mixed cultures of dark-and photo-fermentative bacteria using distillers grains. *Int J Hydrogen Energy* 2016;41:2377–82.
- [8] Marone A, Ayala-Campos OR, Trably E, Carmona-Martinez AA, Moscoviz R, Latrille E, et al. Coupling dark fermentation and microbial electrolysis to enhance bio-hydrogen production from agro-industrial wastewaters and by-products in a bio-refinery framework. *Int J Hydrogen Energy* 2017;42:1609–21.
- [9] Trchounian K, Sargsyan H, Trchounian A. H<sub>2</sub> production by *Escherichia coli* batch cultures during utilization of acetate and mixture of glycerol and acetate. *Int J Hydrogen Energy* 2015;40:12187–92.
- [10] Dharmadi Y, Murarka A, Gonzalez R. Anaerobic fermentation of glycerol by *Escherichia coli*. A new platform for metabolic engineering. *Biotech Bioeng* 2006;94:821–9.
- [11] Trchounian K, Trchounian A. Hydrogenase 2 is most and hydrogenase 1 is less responsible for H<sub>2</sub> production by *Escherichia coli* under glycerol fermentation at neutral and slightly alkaline pH. *Int J Hydrogen Energy* 2009;34:8839–45.
- [12] Thapa LP, Lee SJ, Yang XG, Yoo HY, Park C, Kim SW, et al. Co-fermentation of carbon sources by *Enterobacter aerogenes* ATCC 29007 to enhance the production of bioethanol. *Bioproc Biosyst Eng* 2014;37:1073–84.
- [13] Trchounian K, Sargsyan H, Trchounian A. Hydrogen production by *Escherichia coli* depends on glucose concentration and its combination with glycerol at different pHs. *Int J Hydrogen Energy* 2014;39:6419–23.
- [14] Wang M, Yu C, Zhao H. Directed evolution of xylose specific transporters to facilitate glucose-xylose co-utilization. *Biotechnol Bioeng* 2016;113:484–91.
- [15] Trchounian K, Müller N, Schink B, Trchounian A. Glycerol and mixture of carbon sources conversion to hydrogen by *Clostridium beijerinckii* DSM791 and effects of various heavy metals on hydrogenase activity. *Int J Hydrogen Energy* 2017;42:7875–82.
- [16] Zagrodnik R, Łaniecki M. The effect of pH on cooperation between dark-and photo-fermentative bacteria in a co-

- culture process for hydrogen production from starch. *Int J Hydrogen Energy* 2017;42:2878–88.
- [17] Moscoviz R, Trably E, Bernet N. Consistent 1, 3-propanediol production from glycerol in mixed culture fermentation over a wide range of pH. *Biotechnol Biofuels* 2016;9:32.
- [18] Hitit ZY, Lazaro CZ, Hallenbeck PC. Hydrogen production by co-cultures of *Clostridium butyricum* and *Rhodospseudomonas palustris*: optimization of yield using response surface methodology. *Int J Hydrogen Energy* 2017;42:6578–89.
- [19] Trchounian K, Poladyan A, Vassilian A, Trchounian A. Multiple and reversible hydrogenases for hydrogen production by *Escherichia coli*: dependence on fermentation substrate, pH and the  $F_0F_1$ -ATPase. *Crit Rev Biochem Mol Biol* 2012;47:236–49.
- [20] Pinske C, Jaroschinsky M, Linek S, Kelly CL, Sargent F, Sawers RG. Physiology and bioenergetics of [NiFe]-hydrogenase 2-catalyzed  $H_2$ -consuming and  $H_2$ -producing reactions in *Escherichia coli*. *J Bacteriol* 2015;197:296–306.
- [21] Bagramyan K, Mnatsakanyan N, Poladian A, Vassilian A, Trchounian A. The roles of hydrogenases 3 and 4, and the  $F_0F_1$ -ATPase, in  $H_2$  production by *Escherichia coli* at alkaline and acidic pH. *FEBS Lett* 2002;516:172–8.
- [22] Trchounian K, Trchounian A. Hydrogen producing activity by *Escherichia coli* hydrogenase 4 (*hyf*) depends on glucose concentration. *Int J Hydrogen Energy* 2014;39:16914–8.
- [23] Andrews SC, Berks BC, Mcclay J, Ambler A, Quail MA, Golby P, et al. A 12-cistron *Escherichia coli* operon (*hyf*) encoding a putative proton-translocating formate hydrogen lyase system. *Microbiology* 1997;143:3633–47.
- [24] Schlenzog V, Lutz S, Bock A. Purification and DNA-binding properties of FHLA, the transcriptional activator of the formatehydrogenlyase system from *Escherichia coli*. *J Biol Chem* 1994;269:19590–6.
- [25] Self WT, Shanmugam KT. Isolation and characterization of mutated FhlA proteins which activate transcription of the *hyc* operon (formatehydrogenlyase) of *Escherichia coli* in the absence of molybdate. *FEMS Microbiol Lett* 2000;184:47–52.
- [26] Skibinski DAG, Golby P, Chang Y-S, Sargent F, Hoffman R, Harper R, et al. Regulation of the hydrogenase-4 operon of *Escherichia coli* by the  $\sigma^{54}$ -dependent transcriptional activators FhlA and HyfR. *J Bacteriol* 2002;184:6642–53.
- [27] King PW, Przybyla AE. Response of *hya* expression to external pH in *Escherichia coli*. *J Bacteriol* 1999;181:5250–6.
- [28] Trchounian K, Pinske C, Sawers G, Trchounian A. Characterization of *Escherichia coli* [NiFe]-hydrogenase distribution during fermentative growth at different pHs. *Cell Biochem Biophys* 2012;62:433–40.
- [29] de Oliveira Faber M, Ferreira-Leitão VS. Optimization of biohydrogen yield produced by bacterial consortia using residual glycerin from biodiesel production. *Bioresour Technol* 2016;219:365–70.
- [30] Trchounian K, Poladyan A, Trchounian A. Optimizing strategy for *Escherichia coli* growth and hydrogen production during glycerol fermentation in batch culture: effects of some heavy metal ions and their mixtures. *Appl Energy* 2016;177:335–40.
- [31] Gabrielyan L, Hakobyan L, Trchounian A. Comparative effects of Ni (II) and Cu (II) ions and their combinations on redox potential and hydrogen photoproduction by *Rhodobacter sphaeroides*. *J Photochem Photobiol B Biol* 2016;164:271–5.
- [32] Valle A, Cabrera G, Cantero D, Bolivar J. Identification of enhanced hydrogen and ethanol *Escherichia coli* producer strains in a glycerol-based medium by screening in single-knock out mutant collections. *Microb Cell Fact* 2015;14:93.
- [33] Wang Y, Zhou P, Tong J, Gao R. Advances in the genetic modification of *Rhodobacter sphaeroides* to improve hydrogen production. *Renew Sustain Energy Rev* 2016;60:1312–8.
- [34] Trchounian K, Soboh B, Sawers RG, Trchounian A. Contribution of hydrogenase 2 to stationary phase  $H_2$  production by *Escherichia coli* during fermentation of glycerol. *Cell Biochem Biophys* 2013;66:103–8.
- [35] Baba T, Ara T, Hasegawa M, Takai Y, Okumura Y, Baba M, et al. Construction of *Escherichia coli* K-12 in-frame, single-gene knockout mutants: the Keoi collection. *Mol Syst Biol* 2006;2. 2006.0008.
- [36] Mnatsakanyan N, Bagramyan K, Trchounian A. Hydrogenase 3 but not hydrogenase 4 is major in hydrogen gas production by *Escherichia coli* formate hydrogen lyase at acidic pH and in the presence of external formate. *Cell Biochem Biophys* 2004;41:357–66.
- [37] Gabrielyan L, Sargsyan H, Hakobyan L, Trchounian A. Regulation of hydrogen photoproduction in *Rhodobacter sphaeroides* batch culture by external oxidizers and reducers. *Appl Energy* 2014;131:20–5.
- [38] Beliushtin AA, Pisarevsky AM, Lepnev GP, Sergeyev AS, Shultz MM. Glass electrodes: a new generation. *Sens Actuator B Chem* 1992;10:61–6.
- [39] Fernandez VM. An electrochemical cell for reduction of biochemical: its application to the study of the effect of pH and redox potential on the activity of hydrogenases. *Anal Biochem* 1983;130:54–9.
- [40] Eltsova ZA, Vasileva LG, Tsygankov AA. Hydrogen production by recombinant strains of *Rhodobacter sphaeroides* using a modified photosynthetic apparatus. *Appl Biochem Microbiol* 2010;46:487–91.
- [41] Noguchi K, Riggins DP, Eldahan KC, Kitko RD, Slonczewski JL. Hydrogenase-3 contributes to anaerobic acid resistance of *Escherichia coli*. *PLoS One* 2010;5. e10132.
- [42] Piskarev IM, Ushkanov VA, Aristova NA, Likhachev PP, Myslivets TS. Establishment of the redox potential of water saturated with hydrogen. *Biophysics* 2010;55:13–7.
- [43] Maeda T, Wood TK. Formate detection by potassium permanganate for enhanced hydrogen production in *Escherichia coli*. *Int J Hydrogen Energy* 2008;33:2409–12.
- [44] Trchounian A, Sawers G. Novel insights into the bioenergetics of mixed-acid fermentation: can hydrogen and proton cycles combine to help maintain a proton motive force? *IUBMB Life* 2014;66:1–7.
- [45] Sawers RG, Blokesch M, Böck A. Anaerobic formate and hydrogen metabolism. *EcoSal Plus* 2004 Sep 9;1(1).
- [46] Maeda T, Sanchez-Torres V, Wood TK. *Escherichia coli* hydrogenase 3 is a reversible enzyme possessing hydrogen uptake and synthesis activities. *Appl Microbiol Biotechnol* 2007;76:1036–42.
- [47] Hube M, Blokesch M, Böck A. Network of hydrogenase maturation in *Escherichia coli*: role of accessory proteins HypA and HybF. *J Bacteriol* 2002;184:3879–85.
- [48] Forzi L, Sawers RG. Maturation of [NiFe]-hydrogenases in *Escherichia coli*. *Biomaterials* 2007;20:565–78.
- [49] Trchounian K, Sanchez-Torres V, Wood TK, Trchounian A. *Escherichia coli* hydrogenase activity and  $H_2$  production under glycerol fermentation at a low pH. *Int J Hydrogen Energy* 2011;36:4323–31.